

WHAT IS CLAIMED IS:

1. An interpolymeric carrier concentrate comprising (a) a non-volatile oil suspension medium, (b) an oil soluble polymer physically entrapped in a network of (c) a water insoluble, crosslinked polymer selected from the group consisting of a polymer of a vinyl lactam, a vinylamide, an acrylic acid, an alkyl acrylate, an alkyl acrylamide and mixtures thereof.
2. The carrier of claim 1 wherein (c) is a polymer derived from a vinyl pyrrolidone and acrylic acid.
3. The carrier of claim 1 wherein (c) is a polymer derived from a C₁ to C₃₀ alkyl acrylate or mixture of said acrylates.
4. The carrier of claim 1 wherein (b) is a polymeric mixture of vinyl pyrrolidone and acrylic acid.
5. The carrier of claim 1 wherein (b) is a polymeric mixture of C₁ to C₃₀ alkyl acrylates.
6. The carrier of claim 1 wherein the weight ratio of (b) to (c) is between about 10:1 and 1:10.
7. The carrier of claim 6 wherein the weight ratio of (b) to (c) is between about 2:1 and 1:2.

8. The carrier of claim 1 wherein said oil is an organic suspension agent.
9. The carrier of claim 8 wherein said oil isocetyl stearate.
10. The carrier of claim 1 wherein (c) is crosslinked between about 0.5-5 wt.%.
11. The carrier of claim 1 wherein (c) is crosslinked with pentaerithritol triallyl ether.
12. The carrier of claim 1 which optionally and additionally contains a surfactant and/or a dispersant in an effective distributing amount for the active component.
13. The process of preparing the carrier of claim 1 which comprises:
 - i. under anhydrous conditions, in a first reaction stage, introducing a first polymerizable, crosslinkable monomer A and between about 0.05 and about 5 wt.% based on monomer of a crosslinking agent into a reactor containing about 25 to about 80 wt.% of a liquid, non-volatile oil;
 - ii. polymerizing and crosslinking monomer A, in the presence of a free radical polymerization initiator and said crosslinking agent at a temperature of from about 40°C to about 160°C for a period of from 1 to 12 hours to form a polymeric network;
 - iii. in a second reaction stage, gradually introducing a distinctly different monomer B into the reactor under constant agitation sufficient to allow monomer B to penetrate and enter said.

- preformed network and polymerizing monomer B in the preformed network of crosslinked polymer A in the presence of a free radical polymerization initiator at about the same temperature for an additional period of from 1 to 12 hours and
- iv. cooling and recovering the resulting interpolymeric product of the reaction.

14. The process of claim 13 wherein free radical initiator is incrementally introduced during the first and the second stages of the reaction.

15. The process of claim 13 wherein individual initiators for monomers A and B are employed in the first and second stages of the process.

16. The process of claim 13 wherein the same initiator is employed for monomers A and B in the first and second stages of the process.

17. The process of claim 13 wherein monomer B is crosslinked with a crosslinking agent.

18. The process of claim 17 wherein the crosslinking agent for monomer B is the same as the crosslinking agent for monomer A.

19. The process of claim 17 wherein the crosslinking agent for monomer B is different from the crosslinking agent of monomer A.

20. The carrier concentrate of claim 1 wherein crosslinked polymer A is derived from a monomeric mixture of a vinyl lactam and acrylic acid or a mixture of C₁₋₃₀ alkyl acrylates.

21. The carrier concentrate of claim 1 wherein crosslinked polymer A is derived from a monomeric mixture of vinyl lactam and acrylic acid.

22. The carrier concentrate of claim 1 wherein the non-volatile oil is isocetyl stearate.

23. The carrier of claim 1 wherein said crosslinking agent in the first stage of the crosslinking reaction is pentaerythritol triallyl ether.

24. An emulsion or gel of the concentrate carrier of claim 1 homogenized with between about 20 and about 200 volumes of water/volume concentrate.

25. The emulsion of claim 24 wherein the volume of water is between 30 and 100.

26. The concentrate carrier of claim 1 wherein an active cosmetic or pharmaceutical component is added to the carrier concentrate in an amount up to about 20 wt.% and said concentrate optionally contains less than 10 wt.% of an actively inert excipient selected from the group consisting of a thickener, a moisturizer, a dispersing agent or a mixture thereof.

27. The concentrate carrier of claim 26 wherein said active component is a sun blocking agent.

28. The concentrate carrier of claim 1 wherein the weight ratio of monomer A to monomer B is between about 1:10 and about 10:1.

29. The concentrate carrier of claim 1 wherein the weight ratio of monomer A to monomer B is between about 1:2 and about 2:1.

30. The process of claim 13 wherein at least one of the monomers fed to the reactor is homogenized in a non-volatile oil.

31. The process of claim 13 wherein the product of the process is acidic and is mixed with a base before dilution with water to form an emulsion.

32. The process of claim 13 wherein an effective cosmetically active amount of a personal care component is added to the product of the process.

33. The process of claim 32 wherein the cosmetically active component is a sun blocking agent.

34. The process of claim 13 wherein the product of the process contains an effective dispersing amount of a surfactant for said active component.

35. The process of claim 13 wherein said product is homogenized with between about 20 and about 200 volumes of water/volume of concentrate.